



Technology Description (TD) for Anaerobic Digestion Technologies

Contact Information:

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|---|--------------------------------|--|------------------|--------|
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| <i>Date (of filling the TD):</i> | 08.09.2017 (Update) | | | |

Technology Description:

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|--|---|
| NAME OF TECHNOLOGY | Reactor for biomass digestion |
| ASSIGNMENT OF TECHNOLOGY | Reactor for biomass digestion with innovation mixing system |
| TECHNICAL READINESS LEVEL | <p>1 2 3 4 5 6 7 8 9</p> |
| <p>TRL 1 - basic principles observed TRL 2 - technology concept formulated TRL 3 - experimental proof of concept TRL 4 - technology validated in lab TRL 5 - technology validated in relevant environment (industrially relevant environment in case of key enabling technologies) TRL 6 - technology demonstrated in relevant environment (industrially relevant environment in case of key enabling technologies) TRL 7 - system prototype demonstration in an operational environment TRL 8 - system completed and qualified TRL 9 - actual system proven in operational environment (competitive manufacturing in the case of key enabling technologies; or in space)</p> | |
| What is the core innovation? (Please | Cage mixing system ensures better biogas release, removes foam from reactor and |



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| explain here what is innovative on this technology and which problem does the technology solve.) | mechanically grinds the substrate. | |
| Vision of the innovation (Please describe here what impact you see for the future) | Solution can compete with the currently existing system which are dedicated to small biogas plant. | |
| What are the R&D needs for your technology? (Are there any barriers or challenges which still need to be overcome?) | The barrier is the lack of installations of this kind in technical scale. Necessary development of the prototype on a semi-technical scale and selection and optimization of operating parameters. | |
| TECHNOLOGY/EQUIPMENT AVAILABILITY | technology licence sellers Technology supplier has a prototype functioning in technical scale. It is possible to test the technology for potential customers. The technology supplier is not a producing company. | |
| PATENT RIGHTS | YES/ NO | |
| METHOD OF MAKING THE TECHNOLOGY AVAILABLE | <i>Licence selling</i> | YES/ NO |
| | <i>Licence granting</i> | YES/ NO |
| POSSIBLE END USERS OF TECHNOLOGY | <i>Please name end users/ contacts that should be invited to project workshops</i> | Biogas plant operators |

Description of the technology/equipment:

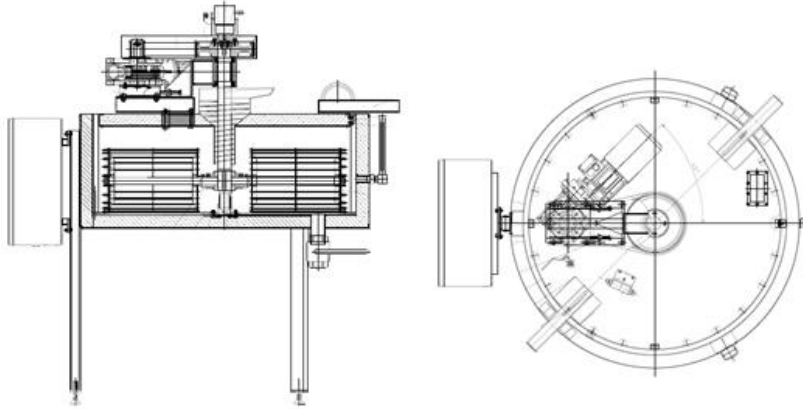
Reactor for biomass digestion with innovation mixing system

The reactor is a tubular tank with internal diameter of $D = 1.2$ m and height of $H = 0.4$ m.

Operating height, filled with anaerobic sludge, is $H_{op} = 0.3$ m. Above, the gas phase is present, in which biogas is collected. In order to provide anaerobic conditions, the reactor is a closed with a dome, which the side walls are located below the liquid level in the reactor. (Fig. 1).



Fig. 1 Scheme of reactor for biomass digestion with mixing cages



The side walls, the bottom and the dome of the reactor are insulated with a layer of polystyrene with a thickness of 5.0 cm. In the bottom of the reactor the heating system is installed, with the possibility of controlling the temperature in the reactor. On the dome, the feed supply valve and the gas valve are located, by which organic substrate is introduced and the biogas is discharged, respectively. In the bottom of the reactor, there is a valve to discharge of the sludge.

Mixing system of the reactor consist of two cylindrical stirrers in the form of cage with diameter of = 0.35 cm. Cages by doing rotation around the axis of the reactor at the same time turn against its own axis. The rotational speed about the axis of the reactor was regulated in the range of 0 to 5 rpm.

Parameters of anaerobic reactor:

Internal diameter $D_w = 1200$ mm

Outer diameter $D_z = 1300$ mm

Operating height $H_{op} = 300$ mm

Internal height $H_w = 400$ mm



Active volume $V_{ac} = 339 \text{ L}$

Volume of the gas phase $V_g = 113 \text{ L}$

Diameter of the mixing cage $D_k = 350 \text{ mm}$

Amount of mixing cages 2

Speed range $v = 0 - 5 \text{ rpm}$



Fig. 2 Reactor for biomass digestion with innovation mixing system

The construction of the reactor was developed under the Key project entitled “Model agro-energy complexes as an example of distributed cogeneration based on local renewable energy sources” POIG.01.01.02-00-016/08 as part of the Innovative Economy Operational Program 2007-2013, as well as from the European Regional Development Fund.



Technical Data

| Parameter | | Value (please fill or tick) If value not available, please give estimate (and indicate with *). | Comments (e.g. which condition does the entered value correspond to?) |
|---|--|---|---|
| <i>Current technology</i> | Biogas production rate of technology at current TRL-level (Nm ³ /h) | 0.012 – 0.030 | |
| <i>Data basis for following data list</i> | 1.: market ready stage of technology (based on test runs of current techn.) | 1 <input type="checkbox"/> (preferably) | |
| | <u>Please only use 2. or 3. if 1. not at all possible.</u> | | |
| | 2.: market ready stage of technology (based on estimate) | 2 <input type="checkbox"/> | |
| | 3.: current level (TRL) of technology | 3 <input checked="" type="checkbox"/> | |
| <i>Technical efficiency</i> | Methane content in biogas (%) | 50-70% | Depending on the substrate |
| <i>Capacity</i> | Flow rate and type per substrate (Mg/h) | 0.00025-0.00050 | |
| | Biogas production rate (range) (Nm ³ /h) | 0.012 – 0.030 | Depending on the substrate |
| | Possible range for upscaling | up to 300 Nm ³ /day | Technology for little and middle biogas plant |
| <i>Data for assessment of economical added value, possible contribution to GHG-reduction and availability</i> | Fermenter and biogas process technology(e.g. continuously stirred reactor, plug flow digester, box or garage type) | CSTR | |
| | Electricity demand (kWhel/Nm ³ biogas) | 0,9 | |
| | Heat demand (kWhth/Nm ³ biogas) | 1,6 | |
| | Chemical/additives demand (kg/h or kg/Nm ³ biogas) | not necessary | |
| | Demand of other substances (kg/h or kg/Nm ³ biogas) | not necessary | |
| | Temperature in fermenter (°C) | 35 - 60 | |



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|--------------------|---|---|---|
| | Pressure of biogas at exit of fermenter (bar _{abs}) | 0,01 | |
| | m ³ fermenter volume used | 0.1 | |
| | Full load hours (h/a) | 8000 | |
| | Hydraulic retention time (days) | 30 - 60 | |
| | Max. dry matter content (%) | 80 | |
| | Organic loading rate (kg VS/m ³ d) | 2 - 4 | |
| | Space requirement (m ²) | 2 | |
| | Staff requirement (excluding maintenance) (h/a) | 200 | |
| | Specific capital costs (excluding project development, planning, permission and additional building costs) (€/Nm ³ /h) | <p>Please give exact specific cost if possible, if not please specify range.</p> <input type="checkbox"/> < 5.000 €/Nm ³ /h <input checked="" type="checkbox"/> 5.000 - 10.000 €/Nm ³ /h - 10 000 <input type="checkbox"/> 10.000 € - 15.000 €/Nm ³ /h <input type="checkbox"/> > 15.000 €/Nm ³ /h | Not determined on an industrial scale |
| | Maintenance costs (including spare parts, staff) (€/a or €/operating hour) | 200 | Not determined on an industrial scale |
| | Production costs (€/Nm ³ biogas) | 0,2 – 0,5 | Not determined on an industrial scale |
| | Expected lifetime of unit (years) | 15 | |
| <i>Flexibility</i> | Types of substrate (solid and liquid) | Solid and liquid Maize, Cow manure, grass silage | Cage mixing system improving efficiencies of solid substrate fermentation |
| | Start-stop-flexibility | | |



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| | Part-load possibility | <input checked="" type="checkbox"/> Yes, 50 – 100 % of full capacity <input type="checkbox"/> No | |
| | Is self-maintenance of technology possible? | <input checked="" type="checkbox"/> Yes, 80 % of total maintenance hours per year that can be done by operator himself <input type="checkbox"/> No | |
| | Necessity for adaptations of other parts of the plant | not necessary | |
| | Advantages/disadvantages of technology | Advantages during the mixing solid substrate (maize, cow manure, grass silage) is gridded Innovative mixing system, where rolls destroy the structure of the substrate - it also destroys the foam which is not good for the biomass /disadvantages high cost of materials | |
| | Special application area of technology | Technology for substrates with low level of hydration | |